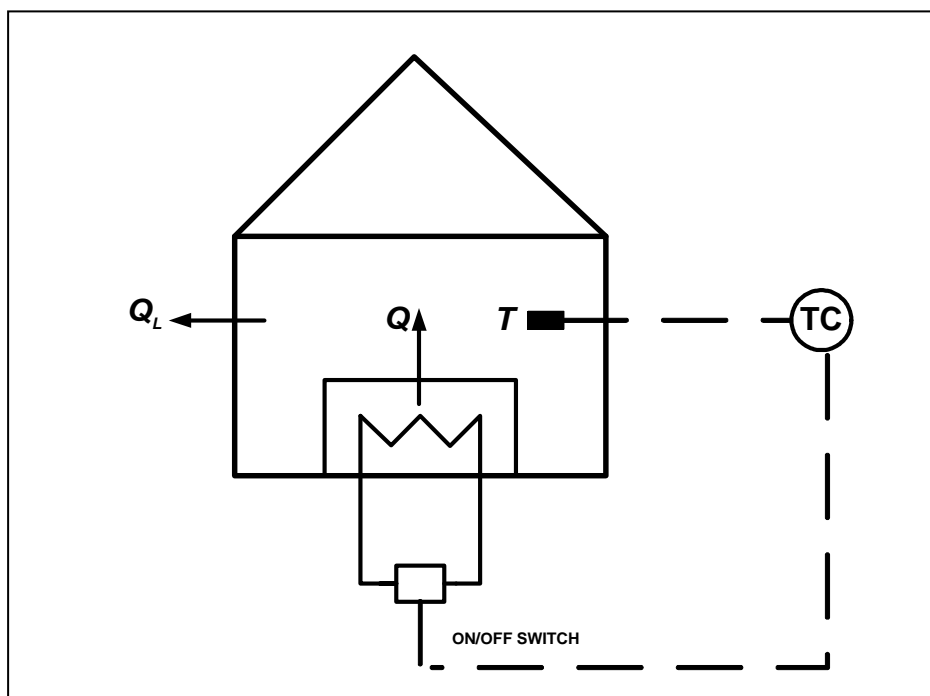


## Chapter 1

1.1

- a) True
- b) True
- c) True
- d) False
- e) True

1.2



**Controlled variable-**  $T$  (house interior temperature)

**Manipulated variable-**  $Q$  (heat from the furnace)

**Disturbance variable-**  $Q_L$  (heat lost to surroundings); other possible sources of disturbances are the loss of gas pressure and the outside door opening.

Specific disturbances include change in outside temperature, change in outside wind velocity (external heat transfer coefficient), the opening of doors or windows into the house, the number of people inside (each one generating and transmitting energy into the surrounding air), and what other electric lights and appliances of any nature are being used.

### 1.3

The ordinary kitchen oven (either electric or gas), the water heater, and the furnace (Ex. 1.2) all work similarly, generally using a feedback control mechanism and an electronic on-off controller. For example, the oven uses a thermal element similar to a thermocouple to sense temperature; the sensor's output is compared to the desired cooking temperature (input via dial or electronic set-point/display unit); and the gas or electric current is then turned on or off depending on whether the temperature is below or above the desired value. Disturbances include the introduction or removal of food from the oven, etc. A non-electronic household appliance that utilizes built-in feedback control is the water tank in a toilet. Here, a float (ball) on a lever arm closes or opens a valve as the water level rises and falls above the desired maximum level. The float height represents the sensor; the lever arm acting on the valve stem provides actuation; and the on-off controller and its set point are built into the mechanical assembly.

### 1.4

No, a microwave oven typically uses only a *timer* to operate the oven for a set (desired) period of time and a *power level* setting that turns the power on at its maximum level for a fixed fraction of the so-called duty cycle, generally several seconds.

Thus setting the Power Level at 6 (60% of full power) and the Cook Time to 1:30 would result in the oven running for a total of one and one-half minutes with the power proportioned at 60% (i.e., turned on 100% for 6 seconds and off for 4 seconds, if the fixed duty cycle is 10 seconds long). This type of control is sometimes referred to as programmed control, as it utilizes only time as the reference variable .

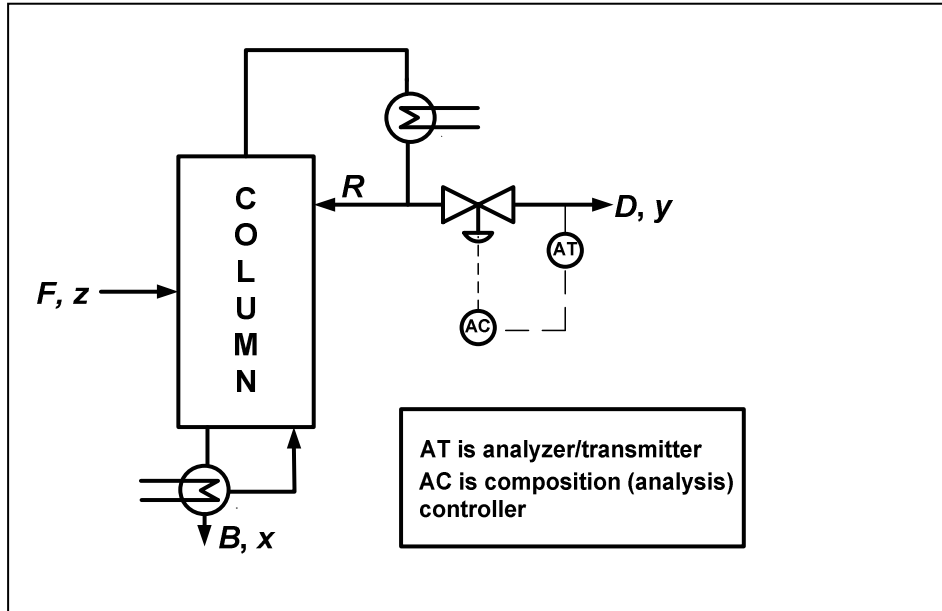
The big disadvantage of such an approach is that the operator (here the cook) has to estimate what settings will achieve the desired food temperature or will cook the food to the desired state. This can be dangerous, as many people can attest who have left a bag of popcorn in the oven too long and set the bag on fire, or embarrassing, as anyone knows who has served a frozen meal that did not quite thaw out, let alone cook. What good cooks do is provide a measure of feedback control to the microwave cooking process, by noting the smell of the cooking food or opening the door and checking occasionally to make sure it is heating correctly. However, anyone who has used a microwave oven to cook fish filets, for example, and blown them all over the oven, learns to be very conservative in the absence of a true feedback control mechanism. [Note that more expensive microwaves do come equipped with a temperature probe that can be inserted into the food and a controller that will turn off the oven when the temperature first reaches the desired (set point) value. But even these units will not truly control the temperature.]

## 1.5

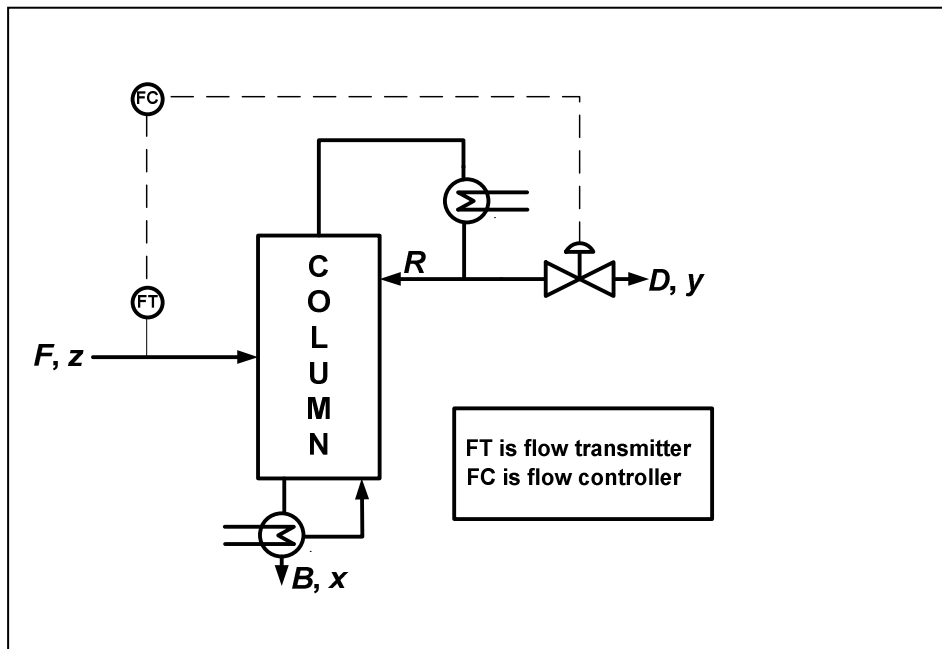
- a) In steering a car, the driver's eyes are the sensor; the driver's hands and the steering system of the car serve as the actuator; and the driver's brain constitutes the controller (formulates the control action i.e., turning the steering wheel to the right when the observed position of the car within its desired path is too far to the left and vice versa). Turns in the road, obstructions in the road that must be steered around, etc. represent disturbances.
- b) In braking and accelerating, a driver has to estimate mentally (on a practically continuous basis) the distance separating his/her car from the one just ahead and then apply brakes, coast, or accelerate to keep that distance close to the desired one. This process represents true feedback control where the measured variable (distance of separation) is used to formulate an appropriate control response and then to actuate the brakes/accelerator according to the driver's best judgment. Feedforward control comes into the picture when the driver uses information other than the controlled variable (separation distance) that represents any measure of disturbance to the ongoing process; included would be observations that brake lights on preceding vehicle(s) are illuminating, that cars are arriving at a narrowing of the road, etc. Most good drivers also pay close attention to the rate of change of separation distance, which should remain close to zero. Later we will see that use of this variable, the time derivative of the controlled variable, is just another element in feedback control because a function of the controlled variable is involved.

1.6

- a) Feedback Control : Measured variable:  $y$   
 Manipulated variable:  $D, R$ , or  $B$  (schematic shows  $D$ )



- b) Feedforward Control: Measured variable:  $F$   
 Manipulated variable:  $D$  (shown),  $R$  or  $B$

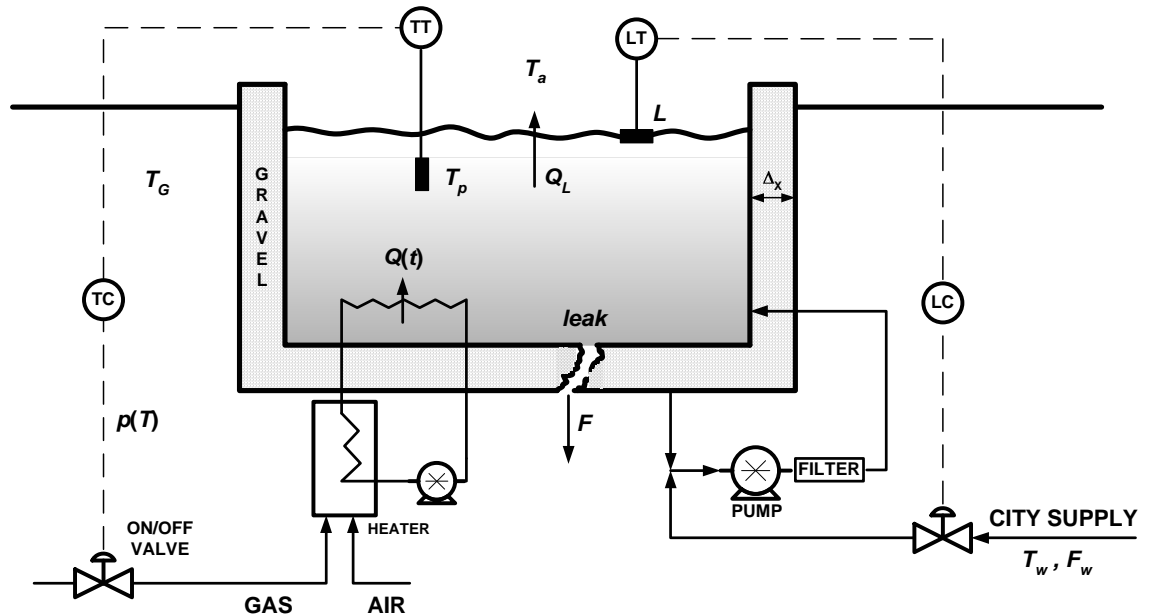


1.7

Both flow control loops are feedback control systems. In both cases, the controlled variable (flow) is measured and the controller responds to that measurement.

1.8

a)



**Outputs:**  $T_p$ ,  $L$ (level)

**Inputs:**  $Q(t)$ ,  $F_w$

**Disturbances:**  $T_w$ ,  $T_a$

- b) Either  $T_w$  or  $T_a$  or both can be measured in order to add feedforward control.
- c) Steady-state energy balance

$$Q(t) = UA(T_p - T_a) + k_G \frac{(T_p - T_G)}{\Delta x} + F_w \rho C (T_p - T_w)$$

Laplace transforming the input function, a constant,

$$C_i(s) = \frac{\bar{c}_i}{s}$$

so that

$$sVC(s) + qC(s) = q\frac{\bar{c}_i}{s} \quad \text{or} \quad C(s) = \frac{q\bar{c}_i}{(sV + q)s}$$

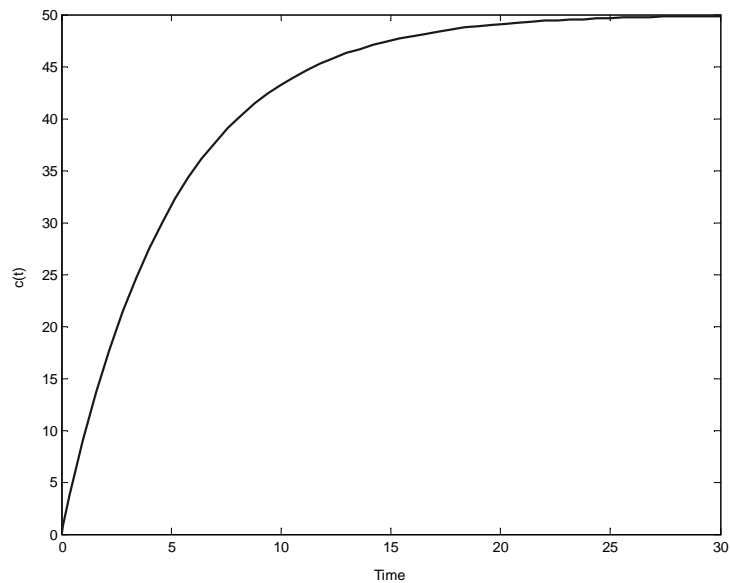
Dividing numerator and denominator by  $q$

$$C(s) = \frac{\bar{c}_i}{\left(\frac{V}{q}s + 1\right)s}$$

Use Transform pair #3 in Table 3.1 to invert ( $\tau = V/q$ )

$$c(t) = \bar{c}_i \left( 1 - e^{-\frac{V}{q}t} \right)$$

Using MATLAB, the concentration response is shown in Fig. S3.17.  
(Consider  $V = 2 \text{ m}^3$ ,  $C_i = 50 \text{ Kg/m}^3$  and  $q = 0.4 \text{ m}^3/\text{min}$ )



**Figure S3.17.** Concentration response of the reactor effluent stream.

$$\frac{C'_m(s)}{C'(s)} = \frac{K}{\tau s + 1} \quad , \quad K = (3-0)/3 = 1 \quad , \quad \tau \approx 6 \text{ sec} = 0.1 \text{ min}$$

(from the graph)

$$\frac{C'_m(s)}{C'_1(s)} = \frac{1}{(0.1s + 1)} \frac{0.5}{(49s + 1)} = \frac{0.5}{(0.1s + 1)(49s + 1)}$$

b)  $C'_1(s) = \frac{3}{s}$

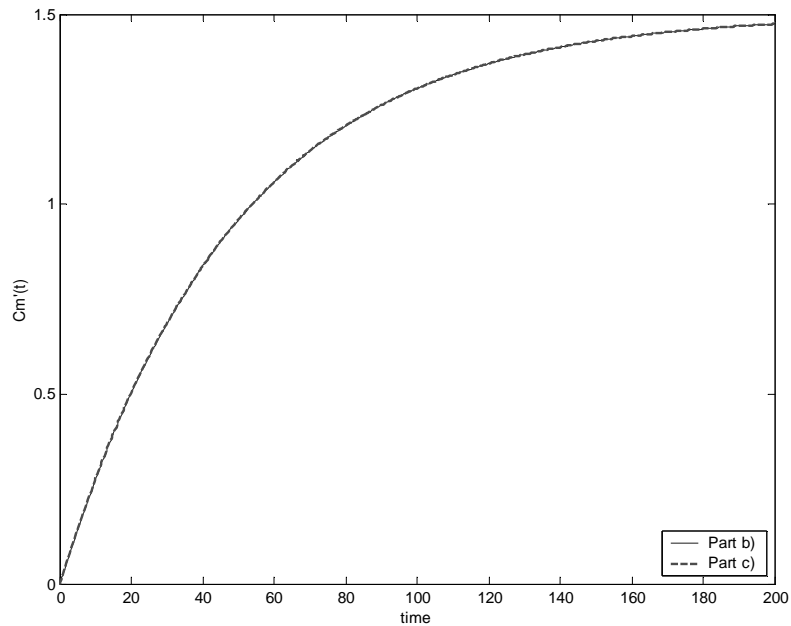
$$C'_m(s) = \frac{1.5}{s(0.1s + 1)(49s + 1)}$$

$$c'_m(t) = 1.5 \left[ 1 + \frac{1}{(49 - 0.1)} (0.1e^{-t/0.1} - 49e^{-t/49}) \right]$$

c)  $C'_m(s) = \frac{0.5}{(49s + 1)} \frac{3}{s} = \frac{1.5}{s(49s + 1)}$

$$c'_m(t) = 1.5(1 - e^{-t/49})$$

- d) The responses in b) and c) are nearly the same. Hence the dynamics of the conductivity cell are negligible.



**Fig S5.20.** Step responses for parts b) and c)

- (d) Derivative control action reduces the settling time but results in a more oscillatory response.

### 14.13

- (a) From Exercise 14.10,

$$G_v(s) = \frac{5.264}{0.083s + 1}$$

$$G_p(s) = \frac{2}{(0.432s + 1)(0.017s + 1)}$$

$$G_m(s) = \frac{0.12}{(0.024s + 1)}$$

The PI controller is  $G_c(s) = 5 \left( 1 + \frac{1}{0.3s} \right)$

Hence the open-loop transfer function is

$$G_{OL} = G_c G_v G_p G_m$$

Rearranging,

$$G_{OL} = \frac{6.317s + 21.06}{1.46 \times 10^{-5} s^5 + 0.00168s^4 + 0.05738s^3 + 0.556s^2 + s}$$



24.5

- a) Using the same methods as described in solution 24.3, the resulting gain matrix is:

Gain Matrix	$w_1$	$w_2$	$w_6$	$w_8$	$w_3$
$w_4$	5.762E-3	4.760E-3	0	5.831E-3	-1.285E-2
$x_{8D}$	5.554E-6	4.558E-6	0	5.445E-6	-9.130E-6
$x_{4A}$	-2.905E-6	-2.398E-6	0	-2.944E-6	6.542E-6
$H_T$	-2.137	-1.927	-1	-10.12	8.829
$H_R$	1	1	0	1	-1

All variables are integrating

The resulting RGA does not provide useful insight for the preferred controller pairing due to the nature of these integrating variables.

- b) Results similar to those obtained in Exercise 24.3 can be obtained with an added loop for reactor level using the  $w_3$  flow rate as the manipulated variable. Both P and PI controllers yield relatively constant reactor level. The quality variable,  $x_{4A}$ , cannot be controlled as tightly however. The responses with P-only control are only slightly different as compared to PI control, which means that zero-offset control on the reactor volume is not necessary for reliable plant operation.

Controller parameters used for variable reactor holdup simulation:

Loop	Gain ( $K_c$ )	Integral Time ( $\tau_I$ )
$w_4-w_1$	1	1
$x_{TD}-w_2$	-6300	1
$x_{4A}-w_8$	-200000	1
$H_T-w_6$	-3.5	1
$H_R-w_3$	-10	1*

\* For PI control